Amendment dated January 17, 2006
Reply to Office Action of October 17, 2005

**AMENDMENTS TO THE CLAIMS** 

1. (Currently Amended) An apparatus for producing hydrophobic silica fine

powder, comprising:

a means for pyrolyzing a silane compound to form silica fine powder,

a means for agglomerating the silica fine powder,

a first cyclone and a first filter for collecting the agglomerated silica fine powder,

a fluidization vessel having a hydrophobizing section or device for hydrophobizing

the collected silica fine power and a deacidifying section or device for removing halogen gas

which accompanies the silica from the hydrophobizing section, and

a second cyclone and a second filter for collecting hydrophobic silica fine powder

which flies out of the fluidization vessel including both the hydrophobizing section or the

device for hydrophobizing and the deacidifying section or the device for removing halogen

gas, and for returning the collected hydrophobic silica to the deacidifying section or device,

which wherein the second cyclone and second filter can each be held at a temperature of 100

to 500°C.

2. (New) An apparatus for producing hydrophobic silica fine powder, comprising:

a combustion chamber for pyrolyzing a silane compound to form silica fine powder,

an agglomerator for agglomerating the silica fine powder,

a first cyclone and a first filter for collecting the agglomerated silica fine powder,

3 ADM/mao

Application No. 10/797,037 Amendment dated January 17, 2006 Reply to Office Action of October 17, 2005

a fluidization vessel having a hydrophobizing section or device for hydrophobizing

the collected silica fine power and a deacidifying section or device for removing halogen

gas which accompanies the silica from the hydrophobizing section, and

a second cyclone and a second filter for collecting hydrophobic silica fine powder

which flies out of the fluidization vessel including both the hydrophobizing section or the

device for hydrophobizing and the deacidifying section or the device for removing

halogen gas, and for returning the collected hydrophobic silica to the deacidifying section

or the device for removing halogen gas, wherein the second cyclone and second filter can

each be held at a temperature of 100 to 500°C.

3. (New)The apparatus of claim 1, wherein the hydrophobizing section or device for

hydrophobizing the collected silica fine power conducts hydrophobizing of the collected

silica fine powder at a temperature of 400 to 600°C and a flow velocity of 1 to 6 cm/s.

4. (New) The apparatus of claim 2, wherein the hydrophobizing section or device

for hydrophobizing the collected silica fine power conducts hydrophobizing of the

collected silica fine powder at a temperature of 400 to 600°C and a flow velocity of 1 to 6

cm/s.

5. (New) The apparatus of claim 1, wherein the decidifying section or device for

removing halogen gas which accompanies the silica from the hydrophobizing section

4 ADM/mao

Application No. 10/797,037 Docket No.: 0171-1068P

Amendment dated January 17, 2006 Reply to Office Action of October 17, 2005

conducts deacidification at a temperature of 400 to 500°C and a flow velocity of 1 to 6

cm/s.

6. (New) The apparatus of claim 2, wherein the decidifying section or device for

removing halogen gas which accompanies the silica from the hydrophobizing section

conducts deacidification at a temperature of 400 to 500°C and a flow velocity of 1 to 6

cm/s.

7. (New) The apparatus of claim 1, wherein the second cyclone and second filter

can each be held at a temperature of 130 to 200°C.

8. (New) The apparatus of claim 2, wherein the second cyclone and second filter

can each be held at a temperature of 130 to 200°C.

5 ADM/mao